

Trends of CCU Technology in Japan and Activities of Nippon Steel Corporation

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Background of CCU

The Agency for Natural Resources and Energy (ANRE) established a new office named the "Carbon Recycling Promotion Office" aiming to promote technological innovations involving capture, storage and utilization of carbon dioxide.



International Conference on Carbon Recycling was just held.

Date and time: In the afternoon of September 25 (Wed.), 2019 Venue: Tokyo metropolitan area Program: Presentations and panel discussions Organizers: METI and NEDO

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Background of CCU



There were calls to accelerate the introduction of various renewable energies — especially hydrogen. The ministers promised to step up existing international efforts to utilize hydrogen, which has long been a goal of Japan in particular.

On fossil fuels, the ministers called for using more liquid natural gas, which produces fewer carbon dioxide emissions than coal. But despite international pressure on the G20 to get out of coal, the ministers continued to show support for coal investment, especially in carbon capture and storage (CCS) and carbon capture and usage (CCU) technologies.

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[G20 Energy and Environment Ministers Meeting]

 Carbon Recycling was unanimously included in the joint statement of the G20 Energy and Environment Ministers Meeting (at Karuizawa).

•Saudi Arabia's proposal "Emissions to Value" was included. The EU, especially Germany, insisted on removing "Carbon Recycling" from the joint statement, but succeeded.

• In Japan / Saudi Arabia, establish a forum for regular discussions on CR technology. The first meeting will be at the CR International Conference on September 25th. Saudi Arabia will be the G20 presidency next year, and CR technology will be on the agenda next year.

 Coal-fired power is necessary to realize the SDGs. Of the G20, we have the support of 19 countries. It is the EU that is isolated.





排出後の処

った動きがある。 一方で世界の発電量の 太陽光や風力が普 |回る。石炭、液化天然ガス



商用化

める。 力が4割で再生エネを上 うち石炭火力は4割を占

有し、 究成果などは出資者で共研究者に資金を出す。研 火力発電は、 CO²の排出が多い石炭 は、欧州を中心に広がる 程の開発につなげる。 きる技術を軸に、企業や 「脱炭素」の流れがある。 ファンド設立の背景に 具体的な製品や工 機閃投資家 が投資対象から外すとい

|供給の両立を||参画する。約1億円で立 ち上げ、 では製造コストが高す 材を作る技術がある。 でコンクリ 材料として、触媒による 力を入れる。CO。を原 別の素材に変える技術に の融資を呼び込んで新た 反応や化学物質との合成 な技術開発に投資する。 これらの技術は現時点 まずはこの。を回収し、 民間資金や銀行 トなどの素 を目指してコスト低減で ぎ、商用ペースの実用化 はできていない。

る。 エネルギ H I 図る。 ステムズ(横浜市)や 力発電が中心のリパワ 呼ぶファンドを立ち上げ 合した三菱日立パワー 作所が火力発電部門を統 がある三菱ケミカルや火 リサイクルファンド」と 16社は近く「カーボン 三菱重工業と日立製 素材分野にノウハウ 川崎重工業などが シ

No. 指す。 進め、 スなどの化石燃料が占め 6割程度は石炭や天然ガ どを作る技術の確立を目 料や建材の素材、 組む。CO"をもとに衣 どから出る二酸化炭素 用する技術の開発で手を (CO")を回収し再利 など16社は、 三菱ケミカルや」パワ CO"の排出抑制を 世界の発電のうち 地球温暖化対策と 発電所な 燃料な

三菱ケミなど 商 用化 1 16 社連

CO²で

| | | せた上で、来年度以降 | 要認力国・地域)エネ | 年度 予算 の に 計 こ し て う 2019: (C |
|---|--|---|--|---|
| 炭素利用、普及に本 | 腰 | したことでありの には利用での 月間での 月 月 日 月 日 日 日 日 日 日 日 日 日 日 日 日 日 | 会合では、国際協力を 会合では、国際協力を 一方、予算に関して 一方、予算に関して | で書きっている 一部である で書きっている |
| 来年度「CO₂→燃料」 | 実証 | 5年物5億 ^ポ | などの事業環境の変化力の小売り全面自由化度は初めて。同社は電 | 51歳安) だった 平均単価は同・ |
| クル」について、普及に向けた取り組みを来年度から本格化させる。火力発電の高効率化経済産業省は、二酸化炭素(CO3)を燃料・製品などに再利用する「カーボンリサイ | では、2016年度か ここの大規模実証事業 市で実施されているC | 関投資家向けに米ドル中国電力は21日、機 | の拡大を進めている。 段の多様化や投資家層 | 数は全国で36- 20月単月の3 |
| R いている。から然母をつくる実正などで青手する。 CCCの実証では、モニタリング手法、や二酸化炭素回収・貯留(CCCS)の大規模実証試験といった既存の事業を発展させ、回 | 入試験が8月までに思ら開始したCO。の圧 | 5億ぷ(約532億円) | 行もこうした取り組み | 39件減)。中7件(前月比) |
| してまとめて計上する見込み。 | にも達成できる見通し 目標の30万シが今年中 計27万シに到達。当初 | 1%。払込期日は27日 た。利率は年2・40 | 達は3500億円を上9年度の長期資金調 | 22件(前月) |
| 「高家勝発」 レジェーン、局加&とと同力と、支持コードマップ・モー乗り出す。 (電源開発)が共同出 FC)の実証事業を通 「カーボンリサイクル」つくる技術の実証にも中国電力と Jパワー 料電池複合発電(1G 省が6月にまとめた」からパイオ燃料などを | するモニタリング手法になった。 | ての社債は今年2月にで、償還期限は202 | 含めて約1232億円 年度の調達額は今回を 限に計画しており、今 | 874件滅)、 業者が1万6 |

- 1. CCU Roadmap in JAPAN
- 2. Activities

in Nippon Steel Corporation

- 3. Blue Carbon Technology
- 4. Conclusions

Roadmap for Carbon Recycling Technologies

June 2019

Ministry of Economy, Trade and Industry

Cooperation of Cabinet Office, Ministry of Education, Culture, Sports, Science and Technology & Ministry of the Environment



CCUS/Carbon Recycling

- Carbon Recycling technology, recognizing carbon dioxide as a source of carbon, capturing and recycling it as raw materials and fuels by mineralization, artificial photosynthetic or Methanation as well as controlling the CO₂ emissions to the air.
- Carbon Recycling technology focuses upon the research and development of CO₂ Utilization in collaboration among industries, academia and governments around the world and promotes disruptive innovation.
- Carbon Recycling is one of key technology for the world together with energy saving, renewable energy and CCS



Roadmap for Carbon Recycling Technologies

Volume level of utilized CO₂

Strategy for Growth strategy based on the Paris Agreement (tentative translation)".



Industry-Academia-Government, or new proposals, and review the roadmap in five years and if needed, as well as taking into account the revision of "Long term

Summary of Carbon Recycling Technology R&D *1 Price researched by secretariat 22 Basic substances, chemicals(excluding some oxygenated compounds), many technologies for fuels require large amounts of inexpensive CO₂-free hydrogens Biomass-derived fuels may require hydrogen for hydrogenation treatment, etc.

| Category | Substance After CO ₂ Conversion | Current Status ^{%1} | Tasks/ Challenges | Price of the Existing Equivalent Product ^{%1} | In 2030 | From 2050 Onwards | |
|----------------------|---|--|---|--|--|--|-------------|
| Basic Substance | Syngas/Methanol, etc. | Partially commercialized. Innovative process (light, electricity utilization) is at R&D stage | Improvement of conversion efficiency and reaction rate, improvement in durability of catalyst, etc. | - | Reduction in process costs | Further reduction in process costs | |
| | Oxygenated Compounds | Partially commercialized (polycarbonates, etc.), Others are at R&D stage [Price example] Price of the existing equivalent product (Polycarbonate) | Reduce the amount of CO2 emission for polycarbonate. Other than polycarbonate, etc. commercialized (Improvement in conversion rate/selectivity, etc.) | Approx. JPY 300- 500/kg (polycarbonate (domestic sale price)) | Costs: similar to those for existing energy/products | Further reduction in costs | |
| Chemicals | Biomass-derived Chemicals | Technical development stage (non-edible biomass) | Cost reduction/effective pretreatment technique, etc. conversion techniques, etc. | — | Costs: similar to those for existing energy/products | Further reduction in costs | |
| | Commodity (olefin, BTX, etc.) | Partially commercialized (Syngas, etc. produced from coal, etc. is utilized) | Improvement in conversion rate/selectivity, etc. | JPY 100/kg (Ethylene (domestic sale price) | _ | Costs: similar to those for existing energy/products | |
| | Liquid Fuel (microalgae biofuel) | Demonstration Stage [Price example] Biojet Fuel: JPY 1600/L | Improvement productivity, cost reduction/ effective pretreatment technique, etc. | JPY 100/L level (bio-jet fuel (domestic sale price)) | Costs: similar to those for existing energy/products (JPY 100-200/L) | Further reduction in costs | |
| Fuels | Liquid Fuel (CO ₂ - derived fuels or biofuels (excluding microalgae-derived ones)) | Demonstration stage (E-Fuel, etc.), partially commercialized for edible biomass-derived bioethanol | Improvement in current processes, system optimization, etc. | JPY 50-80/L (alcohol as raw material (imported price) JPY approx. 130/L Industrial alcohol (domestic sale price) | _ | Costs: similar to those for existing energy/products | |
| | Gas Fuel (Methane) | Demonstration Stage | System optimization, scale-up, etc. | JPY 40-50/Nm ³ (Natural gas (imported price)) | Reduction in costs for CO_2 -derived CH_4 | Costs: similar to those for existing energy/products | |
| Minerals | Carbonates/Concrete products, concrete structures | Partially commercialized. R&D for various technologies techniques are underway towards cost reduction. [Price example] JPY a few 100/t (Road curb Block) | Separation of effective components to respond to CO ₂ , pulverization, etc. | JPY 30/kg (Road curb block (domestic sale price)) | Road curb Block costs: similar to those for existing energy/products | Other products, except road curb block costs: similar to those for existing energy/products | |
| | | | | | | | |
| common Technology | CO ₂ Capture | Partially commercialized (chemical absorption). Other techniques are at research/ demonstration stage [Price example] Approx. JPY4000/t-CO ₂ (Chemical Absorption Technique) | Reduction in the required energy, etc. | _ | JPY 1000-2000/t-CO ₂ level (chemical absorption, solid absorption, physical absorption, membrane separation) | JPY 1000/t-CO₂ or lower | |
| Basic Substance | Hydrogen | Technologies have been roughly established (water electrolysis, etc.) R&D for other techniques are also underway towards cost reduction | Cost reduction, etc. | | JPY 30/Nm ³ | JPY 20/Nm ³ (cost at plant delivery) | 19) ved. |

Scope of Carbon Recycling Technology Roadmap

The carbon recycling technology considers to use CO_2 as resource, thus CO_2 can be utilized even if the replacement of existing products with new ones (resulting from this technology) has occurred in small quantity. Therefore, with cost effectiveness in mind, we continue aiming to allow this technology to be established and spread in as many different fields as possible.

In that case, 2030 shall be set as a relatively-short-term target while 2050 onward as a mid- to long-term target.

| 2030: | Technologies aiming at achieving commercialization (1) Establish an environment where easy utilization CO₂) (2) Technologies which basic technology is establic reducing costs (Products to manufacture do not require inexposition value added which easily replacing existing provide added which easily replacing existing provide added which easily replaced added added which easily replaced added added which easily replaced added ad | on as early a stage as possible. on of CO_2 (reducing costs for capture/recycle of ished, can replace the existing products by ensive hydrogen as well as products with high- oducts) |
|-------|---|---|
| 2050: | Technologies aiming at achieving commercializati Technologies that has not yet been established amount of CO₂ if the technologies have been r (Technologies require utilization of hydrogen at labeled and the second secon | on in the mid- to long-term. ed, but that has great impacts on the use of large ealized low costs) |
| | 2030 (short-term) | 2050 onward (mid-to long-term) |
| Field | Technology requiring no hydrogen and/or high value added products will be commercialized as a start: Chemicals (polycarbonate, etc.) Liquid fuels (bio-jet fuel, etc.) Concrete products (road curb blocks, etc.) | Extended to products that have large demand: Chemicals (commodity: olefin, BTX, etc.) Fuels (gas, liquid) Concrete products (commodity) |

Individual technologies



CCUS/ Carbon Recycling

Carbon Recycling technology, recognizing carbon dioxide as a source of carbon, capturing and recycling it as raw
materials and fuels by mineralization, artificial photosynthetic or Methanation as well as controlling the CO₂ emissions
to the air.



Common technology

CO₂ Capture Technology

- <Technological Challenges>
- Reduction in equipment/operational costs and in required energy

Development of new base materials (absorbents, adsorbents, separation membrane) (for selectivity/capacity/durability improvements) Reduction in production costs of base materials Optimization of processes(in terms of heat/substance/power, etc.)

- Selection of the types of separation and capture techniques based on the CO₂ emission source/use application
- Establishment of CO₂ separation and capture systems suitable for the carbon recycling that ensures cooperation between CO₂ emission sources and demanders/suppliers (co-production)
- Transportation & storage

<Respective Technologies>

• Chemical absorption technique (temperature difference (current process))

Approx. JPY 4,000/t-CO₂

Required energy: Approx.2.5GJ/t-CO $_2$

- Physical absorption technique (pressure difference (demonstration stage))
- Solid absorption technique (temperature difference) (R&D stage)
- Physical adsorption technique (pressure/temperature difference, less advantages from upsizing, improvements in selectivity/capacity/endurance)
- Membrane separation (pressure difference)
- Others include: cryogenic separation technique, Direct Air Capture, etc.
- <Process Technologies to facilitate CO2 Capture>
- Oxygen-enriched/closed IGCC
 Development of low cost oxygen supply technology
- Chemical Looping
 Development of low-cost, long-lasting oxygen carriers

Target for 2030

- For Low-pressure gas (CO₂ separation from flue gas, blast furnace gas, etc.) JPY2,000 level/t-CO₂ Required energy 1.5 GJ/t-CO₂ Chemical absorption, solid absorption, etc.
- For high-pressure gas (CO₂ separation from chemical process/fuel gas, etc.) JPY1,000 level/t-CO₂ Required energy 0.5GJ/t-CO₂ Physical absorption, membrane separation, etc.
- Overall review of other processes Closed IGCC/Chemical looping, etc. JPY1,000 level/t-CO₂ Required energy 0.5GJ/t-CO₂

<Establishing a CO₂ Separation and Catch system>

- Realization of an energy-saving, low cost CO₂ Separation and Catch System that is suitable for each CO₂ emission source/usage
- Realization of 10,000 hour continuous operation8 (to demonstrate the durability & reliability)

Target from 2050 Onwards

- <Commercialization of separation and capture technology>
- Achieve JPY1,000/t-CO₂ or lower
- Improve the durability/ reliability of CO₂ separation and capture systems
- Optimize CO₂ separation and capture systems based on the emission source/the type of operation in the field of application
- Full-fledged spread of CO₂ separation and capture systems

Common technology

• Explanations on CO₂ capture technologies

| Capture technologies | Technology overview | Scope of application |
|----------------------|---|--|
| Chemical absorption | • This is a technology to separate and capture CO_2 , by using a chemical reaction between CO_2 and liquid. | Fire plant/cement/steel & iron/petroleum refinery/chemical industry/natural gas mining |
| Physical absorption | This is a technology to separate and capture CO₂ by dissolving CO₂ into liquid. The absorbing power depends the solubility of CO₂ relative to the liquid used. | Fire plant (high voltage)/petroleum refinery/chemical industry/natural gas mining |
| Solid absorption | This is a technology to separate and capture CO₂ by utilizing solid absorbents. Examples of application of this technology rely on the use of porous materials in which amines, etc. are impregnated (for low temperature separation) or on the use of a solid absorbent that is capable of absorbing CO₂ (for high temperature separation). | Fire plant/cement/petroleum refinery/chemical industry |
| Physical adsorption | • This technology, which utilizes a porous solid such as zeolite, is an adsorption/desorption operation by rising and falling the pressure on the solid (pressure swing) or by rising and falling the temperature on the solid (temperature swing). | Fire plant/steel & iron/cement/ petroleum refinery/chemical industry |
| Membrane separation | • This technology, which utilizes an membrane with separation functions, is a method to separate a target gas (CO_2) from gas mixture, with the aid of the permselectivity of the membrane. | Fire plant (high voltage)/petroleum refinery/chemical industry/natural gas mining |

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Basic substances

Methane Chemistry, etc. ٠ (Until inexpensive Hydrogen will be supplied, use methane (CH4) instead of CO2.)

(1)

P.10

 CO_2 , H_2

Syngas

 CO,H_2

P.11

٠

[CH₄→Syngas (1)]

- Established as a commercial process
- Partial oxidation/ATR, dry reforming: There is a room for improvement, such as making the reaction temperature lower, searching suitable catalysts, improving durability, etc.

[CH₄→Others]

- Separation under high temperature conditions (hydrogen & benzene. etc.)
- Direct synthesis of methanol(2) and of ethylene (3) are still at R& D stage.
- Methane thermal cracking where CO₂-free hydrogen can be obtained is still at R& D stage (catalyst development, carbon removal/utilization technology)

[Wastes→Useful Substances]

- Sophisticate a recycling technology that utilizes waste plastics(physical selection of plastics, removal of impurities, halogen-resistant catalysts, etc.)
- Establishment of industrialized process

<Other Challenges>

Heat management, equipment costs, development of low-cost oxygenation (such as the utilization of oxygen concurrently produced during electrolysis)



CH₃OH

Ethanol

 C_2H_5OH

P.12

P.12

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Fuels

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Basic substances

• Technologies to produce syngas containing Carbon Mono-oxide & Hydrogen

Thermal Chemistry (catalysts, etc.)

- <Technological Challenges>
- Further improvement in current processes (reverse-shift reaction)
 Other Challenges>
- Capture & reuse of the CO₂ produced as a byproduct in reaction system
 Example of specific efforts>
- Thermal cracking of CO₂ utilizing solar heat

Photochemistry (photocatalysts, etc.)

Artificial Photosynthesis (photocatalysts)

- <Technological Challenges>
- Catalyst Development Hydrogen synthesis (photocatalysts) → Reverse shift reaction Direct synthesis of CO

Improvement in conversion efficiency & separation of gas generated <Other Challenges>

- System design of a plant whose commercialization is viable
- Examination & comparison with the current CO production process (methane-derived)

Electrochemistry (electrochemical reduction, etc.)

Artificial Photosynthesis (PV-electrochemical cell)

<Technological Challenges>

- Development of a catalyst electrode that is suitable for high current density (improve reaction rate)
- Development of integration technology for catalyst electrodes (improve the current density per unit volume)
- Production of syngas through co-electrolysis (respond to load change, equipment scale)
- <Other Challenges>
- System design of a plant whose commercialization is viable
- Examination & comparison with the current CO production process (methane-derived)
- Securing reasonable and stable, large amounts of power derived from renewable energy

Synthesis utilizing organisms (such as microorganisms)

Target for 2030

<Conversion Efficiency

- (Photochemistry)>
- Solar energy conversion efficiency: 10% achievement

<Reaction Rate (Current Density)>

• CO₂ processing speed 6t/yr/m²

(Achievement of current density 500mA/cm² at ordinary temperature/normal pressure, electrolytic efficiency50%) (Electrochemistry) ^{Note 1})

<Catalysts>

• Further improvement in durability & Reduction in costs

(Others)

- Development of renewable energy combined systems
- Development of hybrid systems (Photo + Electricity, etc.)
- Sector coupling: Demonstrate a case where CO is used as a reducing agent for steelmaking

Target from 2050 Onwards

<Conversion Efficiency (Photochemistry)> Further improvement of conversion efficiency

<Reaction Rate (Current Density)> CO₂ processing speed 11 t/yr/m² (Achievement of current density 1000mA/cm² at ordinary temperature/normal pressure, electrolytic efficiency 50%) (Electrochemistry) ^{Note 1})

(Others)

 Synthesis that utilizes thermal chemistry/photochemistry/ electrochemistry/organisms is the best mix of various reactions/technologies.

Note1) Estimate under the following conditions: 100MW plant, availability factor:16.3%, and JPY 2/kWh. Source of the available factor: Materials owned by ANRE (Agency for Natural Resources and Energy) Note2) Supplying inexpensive CO₂ free Hydrogen is important

Basic Substances

• Technologies to produce Methanol, etc.

Thermal Chemistry(catalysts, etc.)

 $[\text{ CO}_2 \rightarrow \text{Methanol}]$

- <Technical Challenges>
- Reaction at low temperature Catalyst development/improvement in catalyst's conversion rate/selectivity
- · Separation/removal of the water arising from the reaction
- Direct utilization of low quality exhaust gas (at a research stage) Measures against deterioration/improvements of durability of catalysts
 < Other Challenges>
- Examination & comparison with the current practical process (reaction through syngas)
- Utilization of CO₂ in existing methanol production equipment

 $[Syngas \rightarrow Methanol (or DME)]$

<Technical Challenges>

- Improvement of yields in methanol production
- A system for concurrent production of methanol and DME where syngas is used as a raw material (production adjustment technique)

(production adjustment technique)

Photochemistry (photocatalysts, etc.)

Electrochemistry (electrochemical oxidation/reduction, etc.)

Synthesis utilizing organisms(such as microorganisms)

Implement various types of R&D

<Technical Challenges>

- Direct synthesis of formic acid/methanol(by utilizing the protons in water)
- Improvement in reaction rate & efficiency

<Other Challenges>

• Securing reasonable and stable, large amounts of power derived from renewable energy (in the case of utilizing electricity)

<Specific Practical Example>

Demonstration of integrated bioethanol production from syngas (derived from waste incineration facilities) using microorganisms (The technology to be established by 2023: Goal $500 \sim 1,000$ kL/y scale demonstration to be implemented)

X some processes require no further hydrogen

Target from 2050 Onwards

<Common Challenges> Reduction in process cost

Target for 2030

<Others>

- Development of renewable energy combined systems
- Development of hybrid systems (Photo + Electricity, etc.)
- Considering large-scale methanol supply chain
- Apply the technology to existing production systems/secure affinity
- <Challenges to be taken up when methanol is utilized as a raw material>
- Demonstrate the technology for methanol to be used in an actual environment
- Expand mixed utilization of existing fuels and methanol as well as the mixed ratio

<Common Challenges>

• Further reduction in process cost

<Expected Cost>

 The expected costs are roughly equal to those incurred for the product synthesized from natural gas-derived methanol

Supplying inexpensive CO₂ free Hydrogen is important

Chemicals

• Technologies to produce commodity Substances (Olefins, BTX, etc.)

Target for 2030

<Technical Challenges>

[MTO-olefin] (production plants exist)

 Developing catalysts (improvement in conversion rate/selectivity)
 Eg. Controlling generation ratio of Ethylene,

Eg. Controlling generation ratio of Ethylene, propylene, butane, etc.

 Countermeasures against catalyst poisoning (controlling carbon precipitation)

[MTA-BTX] (R&D projects exist)

 Developing catalysts (improvement in conversion rate/selectivity)
 Eg. Controlling generation ratio of Benzene, toluene, xylene, etc.

Regarding MTO and MTA, methanol derived from coal is implemented or under implemented in China.

[Syngas→olefin, BTX]

Basic research level

Developing catalysts (improvement in conversion rate/selectivity)

Eg. Controlling generation ration of Benzene, toluene, xylene, etc.

Suppression of the generation of CO₂ and methane

[MTO-olefin]

<Catalyst>

Establish C2-C4 selective synthesis technology

- Further improvement in yield & Control of selectivity
- Establish a small-pilot-scale process

[MTA-BTX]

<Catalyst>

 Further improvement of yield and control of selectivity

[Syngas -> Olefin, BTX]

<Catalyst>

• Further improvement of yield and control of selectivity

<CO₂ Emission Intensity>

 In LCA, the amount of emissions from the current process (crude oil derived) must be equal to or lower than the CO₂ emission intensity

Target from 2050 Onwards

<Expected Cost>

• The costs are similar to those for existing energy/products

<CO₂ Emission Intensity>

 In LCA, the amount of emissions from the current process (crude oil derived) must be equal to or lower than half of the CO₂ emission intensity

Supplying inexpensive CO_2 free Hydrogen is important

Chemicals

Technologies to produce Oxygenated Compounds

<Technical Challenges>

- Reduce cost in the current process or for commercialization (polycarbonate synthesis, etc.)
- Further reduction of CO₂ emissions
- Reduction in production costs

Basic research level, under low TRL Process (acrylic acid synthesis, etc.)

- Catalyst development (improvement in conversion rate/selectivity)
- Realization of low LCA for reaction partners (such as utilizing biomass/waste plastics, etc.)

<Other Challenges>

 Considering another CO₂ storage technique based on chemicals (such as oxalic acid, etc.)

Target for 2030

Target from 2050 Onwards

<Expected Cost>

 The costs are similar to those for existing energy/products

<CO₂ Emission Intensity>

 In LCA, the amount of emissions from the current process (crude oil derived) must be equal to or lower than the CO₂ emission intensity <Expected Cost>

Further reduction in costs

<CO₂ Emission Intensity>

 In LCA, the amount of emissions from the current process (crude oil derived) must be equal to or lower than half of the CO₂ emission intensity

Oxygenated compounds include (in alphabetical order):

acetic acid and acetic acid ester, acrylic acid, ethanol, ethylene glycol, oxalic acid, polyamide, polyester, polycarbonate, salicylic acid, urethane, etc.



Chemicals

Technologies to produce biomass-derived chemicals

Target for 2030

<Technical Challenges>

(Cellulose-type biomass)

- Low cost, effective pretreatment technique (separation of cellulose, lignin, etc.)
- Establish the related techniques such as dehydration/drying, removal of impurities, etc.
- Production process of high-value added chemicals from non-edible biomass
- Screening & culture techniques for new microorganisms resources
- Utilization of biotechnology (Genome editing/synthesis), establishment of separation/purification/reaction process techniques
- Fermentation technology and catalyst technology that are not susceptible to impurities
- Development of effective materials conversion technologies for biomass materials
- High functionality in biomass-derived chemicals (adding marine biodegradable functions, etc.)

<Other Challenges>

- Establishing integrated production processes (securing production scale, stability in quality, etc.)
- Expanding the scope of target products including derivatives (oxygenated compounds→olefin, etc.)
- Expanding the scope of application of biomass-derived chemicals and verify their economic performance
- · Establishing an effective collection system for biomass materials
- Standardization of biomass-derived chemicals/intermediates



- Utilize edible biomass (mainly, ethanol and amino acid)
 Utilize oils and fats
- ision

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- Bio and waste power generation
- Synthesize high-value added chemicals (functional chemicals)

- <Expected Cost>
- The costs are similar to those for existing energy/products

<CO₂ Emission Intensity>

 In LCA, as compared to alternative petrochemical products (such as oxygenated compounds, etc.), the amount of emissions from the current process (crude oil derived) must be equal to or lower than half of the CO₂ emission intensity

<Others>

- Diversification and high functionality of biomass-derived chemicals (Controlling marine biodegradable functions, etc.)
- Hydrogen is necessary in hydrogenation treatment

Target from 2050 Onwards

Large-scale production (geographically-distributed chemicals production that utilizes papermaking infrastructure/ agriculture & forestry/wastes, etc.)

<CO₂ Emission Intensity>

- In LCA, as compared to alternative petrochemical products (such as olefin, etc.), the amount of emissions from the current process (crude oil derived) must be equal to or lower than half of the CO₂ emission intensity
- Introduction into global markets (Marine biodegradable plastics : JPY 850 billion (Global market share of Japan: 25%))
- Utilize non-edible biomass/microalgae
- Bio power generation (ultimately, BECCS)
- Diversification of biomass chemicals/fuels

Such technological development is also common to that in fuel sector (bioethanol, etc.)
 Cultivation and capturing biomass technologies include marine use as well (fuel sector as well)
 Confidential: (Dr.Koji Saito): 25of Sep 2019: (CSE2019)
 Confidential: (Dr.Koji Saito): 25of Sep 2019: (CSE2019)
 Confidential: (Dr.Koji Saito): 25of Sep 2019: (CSE2019)

Fuels

• Technologies to produce liquid fuel (1) *Microalgae Biofuel (Jet Fuel/Diesel)

Target for 2030

<Expected Cost>

 Bio-jet Fuel: costs: similar to those for existing energy/products, JPY 100-200/L (Currently, JPY1600/L)

<Production Rate>

• 75 L-oil/day ha (Currently, 35 L-oil/day ha)

<CO₂ Emission Intensity>

 With regard to biojet fuels, in LCA, as compared to existing jet fuels, the amount of emissions from the current process (crude oil derived) must be equal to or lower than half of the CO₂ emission intensity

<Others>

- Compliance with fuel standards
- Scale up to the demonstration level and establish the supply chain
- Expand mixed utilization of the liquid fuel and an existing fuel as well as the mixed ratio
- Since hydrogen is used in relatively small amounts for oil reforming, the presence of CO₂ free hydrogen increases the GHG reduction impact

Target from 2050 Onwards

<Expected Cost>

• Further reductions in costs

<CO₂ Reduction Amount>

 Must contribute to 50% CO₂ reduction relative to that for 2005 in aviation sectors

(FYI) If a biojet fuel with a greenhouse gas emission reduction rate of 50% continues to be introduced at 100 thousand kL/yr, a CO_2 reduction of 123 thousand t/yr will be achieved.

<Technical Challenges>

- (Microalgae→Biojet fuel/Biodiesel)
- Improve productivity (culture system/ gene recombination)
- Low cost, effective pretreatment technique
- Establish the related techniques such as dehydration/drying, oil extraction, removal of impurities, etc.
- Develop the technology for utilizing oils/fats residues
- Scale-up (from bench-scale to pilot-scale, followed by demonstration level)
- · Large-scale technological demonstration
- Pursuit of cost reduction

<Other Challenges>

- Expanding the scope of application and verify economic performance
- Establishing an effective collection system for raw materials

*Such technological development is also common to that in the chemicals sector

(High value added products, such as cosmetics and supplements derived from microalgae are partially commercialized)



Fuels

 Technologies to produce liquid Fuel (2) *CO₂-derived Fuel or Biofuel (excluding microalgae-derived fuels) (such as methanol, ethanol, diesel, jet, DMC, OME, etc.)

Target for 2030

<Technical Challenges>

- Improvement in FT Synthesis (current process) (Improvement in conversion rate/selectivity)
- Improvement in other synthetic reaction (current process)

<Other Challenges>

 System's optimization (Renewable energy introduction (E-Fuel))

<Specific Practical Example>

- Demonstration of integrated bioethanol production from syngas (derived from waste incineration facilities) using microorganisms (The technology to be established by 2023: Goal 500-1,000kL/y scale demonstration to be implemented)
 - % some processes require no further hydrogen

<CO₂ Emission Intensity>

 In LCA, the amount of emissions from the current process (crude oil derived) must be equal to or lower than the CO₂ emission intensity

<Other Challenges>

- Wondering what impact a CO₂-derived fuel may have on the regulations/ device/equipment on which naphtha-/crude oil-derived fuels had no effect
- Demonstrate the technology in an actual environment
- Expand mixed utilization of the liquid fuel and existing fuels as well as the mixed ratio

Target from 2050 Onwards

<Expected Cost>

• The costs are similar to those for existing energy/products

<CO₂ Emission Intensity>

 In LCA, the amount of emissions from the current process (crude oil derived) must be equal to or lower than half of the CO₂ emission intensity

Supplying inexpensive CO₂ free Hydrogen is important

Costs for biofuels and target for CO2 emissions, the same as biomass derived chemicals and microalgae biofuels attempt to reduce the cost equivalent to those existing energy/products in 2030 as well as in LCA the amount of emissions from the current process (crude oil derived) must be lower than half of the CO2 emissions intensity.



Fuels

• Technologies to produce gas fuel (Methane)

<Technical Challenges>

Existing Techniques (Sabatier Reaction)

- Long lasting of catalysts
- Thermal management (utilizing the generation of heat)
- Activity management
- Considering scale-up

R&D of Innovative Technology (co-electrolysis, etc.)

[Power to Methane]

- Production of electrolytic methane through coelectrolysis (utilizing city gas, etc.)
- Integrate the synthesis/power generation of electrolytic methane that utilizes CO2
- Improvement of efficiency

<Other Challenges>

- System's optimization (introducing renewable energy)
- Upsizing/cost reduction
- Equipment cost

<Specific Practical Example>

- Commercial scale (125Nm³/h) demonstration that utilizes CO₂ contained in exhaust gas from a cleaning plant
- Development of basic technology towards practicalscale (60 thousand Nm³/h) demonstration of city gas introduction that utilizes coal fire exhaust gas CO₂ contained in coal-fired exhaust gas

Target for 2030

<Expected Cost>

Reduction in costs for CO₂ derived CH₄

<CO₂ Emission Intensity>

 In LCA, the amount of emissions from the current process must be equal to or lower than the CO₂ emission intensity

<Others>

- Demonstrate insertion into gas introduction pipes
- Develop sales channel/use application
- Expand mixed utilization of the gas fuel and an existing fuel as well as the mixed ratio

Target from 2050 Onwards

<Expected Cost>

• The costs are similar to those for existing energy/products

<CO₂ Emission Intensity>

 In LCA, the amount of emissions from the current process (crude oil derived) must be equal to or lower than half of the CO₂ emission intensity

Supplying inexpensive CO₂ free Hydrogen is important



Minerals

• Carbonates, Concrete Products, etc.

<Technical Challenges>

- Separation of effective components (Ca or Mg compounds) from industrial byproducts (such as iron& steel slag, waste concrete, coal ash, etc.) and/or waste minerals, saltwater (lye water) etc. (including the treatment of byproducts arising from the separation process)
- Energy-saving of the pretreatment (for example, pulverization of effective components) that helps to enhance the reactivity with CO₂ (dry process)
- Energy-saving in wet process (inexpensive treatment for waste water containing heavy metals, etc.)
- Development of inexpensive aggregates, admixtures, etc.
- Scale up

<Energy required to fix 1 ton of CO₂ >

• 500 kWh/t-CO₂ (utilizing blast furnace slag, dry process)

<Other Challenges>

- Establish a system from CO₂ emission sources through to production/supply (to optimize CO₂-fixiation amount and economic performance)
- Expand the scope of application and verify economic performance (development & demonstration of the technologies designed to utilize carbonates – verify the scope of application to concrete products, develop high-value added articles such as fluorescent materials, etc.)
- Long-term evaluate the performance as a civil-engineering/ building material as well as organize standards/guidelines

<Specific Practical Example>

• Development of a technology that is used to convert unused industrial byproducts carbonates (coal ash, etc. in which energy-saving of the pretreatment can be relied on)

% Even now, iron and steel slags and coal ash are used as materials for concrete but not in the form of carbonates

Target for 2030

<Expected Cost>

• Road curb blocks: costs are similar to those for existing energy/products

<Energy required to fix 1 ton of CO₂>

 200 kWh/t-CO₂ (regardless of a raw material and reaction process)

<CO₂ Utilization>

• Approx. 10% of Iron & steel slag and coal ash must be converted into carbonates

<Others>

- Large-scale demonstration
- · Pursuit of cost reduction
- · Survey on appropriate sites within/outside the country
- Promotion of demands by providing some incentive (such as procurement for a public work project, etc.)

<Specific Practical Example>

 Expand raw materials (Coal ash, biomass mixed combustion ash, waste concrete, etc. → Iron & steel slag, waste minerals, saltwater utilization (Iye water), etc.)

Target from 2050 Onwards

<Expected Cost>

 Other products: The costs are similar to those for existing energy/products

<CO₂ Utilization>

- Approx. 50% of Iron and stool slag and cool as
 - steel slag and coal ash

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Important points for Carbon Recycling Technologies

- In order to progress R&D for Carbon Recycling technologies effectively, following points need to be considered for the solving climate change issues and security for natural resources.
 - ✓ Inexpensive CO_2 free Hydrogen is important for many technologies
 - ✓ Under the Hydrogen and fuel cells strategy roadmap in Hydrogen Basic Strategy, the target for 2050 is JPY 20/Nm3 at the plant delivery costs
 - Even supplying hydrogen problems exist, 1) R&D for biomass or any other no hydrogen requested technologies need to progress, as well as 2) without waiting for the establishment for hydrogen supply, start any FS or other transitional activities using CH₄ (methane).
 - ✓ Using zero emission power supply is important for Carbon Recycling
 - ✓ Conversion of a stable substance, CO_2 , into other useful substance will require enormous energy inputs.
 - Life Cycle Analysis (LCA) and its valuation are needed, in order to evaluate Carbon Recycling technologies.
 - ✓ Furthermore, reduce the costs for capturing CO_2 .



Flowchart for CO₂ Utilization (for chemicals/fuels/carbonates)



Flowchart: CO₂ Utilization (for Bio-derived fuels/chemicals)



*Reduction reaction or hydrocracking during the process to produce "chemicals, polymer products or composite materials", may require hydrogen.

; Reserved.

- 1. CCU Roadmap in JAPAN
- 2. Activities
 - in Nippon Steel Corporation
- 3. Blue Carbon Technology
- 4. Conclusions

Direct synthesis of Carbonate ester from CO₂

Nippon Steel Corporation Mitsubishi Gas Chemical Co. Inc. Nippon Steel Engineering Co. Ltd.

1. Background/Objective/Abstract

The **carbonic ester** which is used for the raw materials of plastics (e.g. polycarbonates) and lithium batteries electrolytes, etc. has been produced using **phosgene** of deadly poison up to now.

We found that carbonic ester can be directly produced by CO_2 and alcohol under the catalyst and the existence of dehydration agents. It leads to so-called green process, which means production gently with the environment as well as CO_2 emission reduction.

 CO_2 +2ROH→(RO)₂CO (Eq.)



2. Technical Target

- Reaction validation by pilot test equipment
- Feasibility study and commercialization judgement based on engineering data

3. Impact(CO₂ reduction effect, etc.)

➤CO₂ reduction potential which is about 1 Million tons by substituting of the present process for the world amount of propylene carbonate completely.

Thermal conversion to CO from CO₂ for iron ore reduction Nippon Steel Corporation

1 . Background/Objective/Abstract

In the steel manufacturing process, iron ore must be reduced by carbon-based reductant in the blast furnace (Eq.1), it' inevitable to exhaust a great deal of CO_2 . FeOx+H₂,CO→Fe+CO₂+H₂O (Eq.1)

Utilizing hot sensible heat and waste heat in the ironworks, CO_2 in the blast furnace gas can be reacted and converted to CO through CO_2 and carbon (Eq.2) or CO_2 and some hydro carbons (Eq. 3). We aim at CO_2 reduction by carbon-recycling to return CO into blast furnace as reductant of iron ore.

 $\begin{array}{c} \text{CO}_2 + \text{C} \rightarrow 2\text{CO} & (\text{Eq.2}) \\ \text{nCO}_2 + \text{CnHm} \rightarrow 2\text{nCO} + 1/2\text{mH}_2 & (\text{Eq.3}) \end{array}$



2 . Technical Target

- CO conversion ratio from CO₂: Over 30%
- Reaction validation using real gas from the ironworks

3. Impact(CO₂ reduction effect, etc.)

➤CO₂ reduction potential which is about 2 to 3 Million tons by apply for this process in Japan in 2050's.

Hydrogen manufacture using photosynthesis

Nippon Steel Corporation National Institute of Advanced Industrial science and Technology

1 . Background/Objective/Abstract

Although large amount of CO2 emission is inevitable when iron ore usually be reduced by coal, 'zero-carbon steel' will be realized if iron ore can be reduced by hydrogen.

In the past, hydrogen is produced from fossil fuel accompanying with CO2 emission. We aim at less CO2 type hydrogen production due to comparable low electrolysis voltage using photosynthesis. <photocatalyst>

 $2H_2O + 4Fe^{3+} \rightarrow O_2 + 4Fe^{2+} + 4H^+$ < electrolysis > $4Fe^{2+} + 4H^+ \rightarrow 4Fe^{3+} + 2H_3$



2. Technical Target

- Sunlight energy transform efficiency>3%
 Production cost<¥30/Nm³-H₂
 Certification using bench scale test equipment combined photosynthesis and water
 - electrolysis

3. Impact (CO_2 reduction effect, etc.)

➤CO₂ reduction potential which is about 3 Million tons by apply for this system in 2050's.



Direct synthesis of olefins from CO_2

1. Background/Objective/Abstract

Olefins such as ethylene and propylene as starting materials of chemicals are produced by thermal decomposition of naphtha at higher temp. up to now. We found that **olefins** can be directly synthesized by one-pass from CO2 at low/middle temp. instead of two-pass comprised of CO2 to methanol and methanol to olefins., which leads to eco-friendly green process.

 $CO_2 + H_2 \rightarrow 2ROH$, $ROH \rightarrow C_2 = , C_3 = , \cdots$

 $\underline{CO_2 + H_2 \rightarrow C_2 = C_3 \cdots}$

[Schematic figure of this technology]

 $CO_2+H_2 \rightarrow Methanol catalysis \rightarrow Olefins$ Hybrid catalysis 2. Technical Target

 CO2 conversion >60%
 Optimum process design
 Reaction certification and engineering data acquisition using bench scale equipment

3. Impact(CO₂ reduction effect, etc.)

>CO₂ reduction potential which is about 28 Million tons by substituting of the present process for the domestic amount of ethylene and propylene completely.



Photocatalytic conversion to CO from CO₂ for iron

Nippon Steel Corporation Kyushu Institute of Technology

1 . Background/Objective/Abstract

In the past, CO is produced from fossil fuel accompanying with CO2 emission. We aim at no CO2 type CO production using photosynthesis, which will lead to green process.

<Photocatalytic electrode>

 $H_2O \rightarrow O_2$ < CO_2 catalytic reduction electrode> $CO_2 \rightarrow CO_2$ HCOOH



2. Technical Target

 CO₂ conversion > 2%
 Reaction certification and engineering data acquisition using bench scale equipment comprised of flow-type photocatalytic electrolyzed cell.

3. Impact(CO₂ reduction effect, etc.)

➤CO₂ reduction potential which is about 2 to 3 Million tons by apply for this system in Japan in 2050's.



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CO₂ circulation

Global CO₂ annual emissions: 34.1 billon tons of which steel industry: 0.32 billion tons (2015)



CO₂ reduction target using natural ecosystem



Blue carbon is effective CO₂ reduction target for Japan having long coastline.

By-product iron process, steel slag



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Steel slag utilization to marine environmental restoration



Creation of blue carbon ecosystem using steel slag will contribute to CO₂ reduction

in marine environment.

slag

soil

dredged soil

Seaweed bed restoration by steelmaking slag





The fertilizer had been developed based on the iron necessity in the life cycle of kelp.

Field demonstration of the fertilizer



bout 1 ha seaweed bed were restore by the fertilizer for 10 years.

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Mesocosm for the calculating CO₂ fixed amount





Creating a blue carbon ecosystem using steelmaking slag



NIPPON STEEL

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Introduction

- > Over 1.8 billion tons of worldwide steel production population/economic growth ... steel demand increase
- Carbon-reduction ... large amount of CO2 emission
- Steel production from iron ore is still needed in 2100
- Nov. 2014 : JISF
 Commitment to a Low Carbon Society Phase II
 2030 target ... JPN's NDC (medium-term target)
- ≻ Nov. 2018 : JISF

Long-term vision for climate change mitigation **"A challenge towards Zero-carbon STEEL"** beyond 2030 ... JPN's long-term strategy Hydrogen ... a vital measure

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Pathways towards Zero-carbon STEEL

Pathway 1: Carbon usage and treatment $1/2Fe_2O_3 + 3/4C \implies Fe + 3/4CO_2 \cdot \cdot \cdot GHG$

CCS/CCU is needed

Proven Existing **Experienced**

Exothermic reaction

Pathway 2: Carbon avoidance by hydrogen $1/2Fe_2O_3 + 3/2H_2 \rightarrow Fe + 3/2H_2O \cdots water$ A huge amount of carbon-free hydrogen supply Unproven Unexisting

with rational cost is needed

Inexperienced **Endothermic reaction**

Roadmap for Zero-carbon STEEL

- ✓ JISF has decided to develop super innovative technologies to realize zerocarbon STEEL.
- \checkmark Hydrogen replacing carbon and CO₂ capture are main measures.
- \checkmark COURSE50 is the first step to the future.
- ✓ For hydrogen-reduction, massive and stable supply of carbon-free hydrogen with rational cost is essential.

| s specific in iron & steel sector | 2020 | 2030 |) 204 | 0 20 | 50 | 2100 |
|--|---|--|--|---|---|--|
| Raising ratio of H2-reduction in blast furnace using internal H2 (COG) Capturing CO2 from blast furnace gas for storage | R&D | Impl | ement | ation | | |
| Further H2-reduction in blast furnace by adding H2 from outside (assuming massive carbon-free H2 supply becomes available) | Stepping up | R&D | | | | |
| H2-reduction ironmaking without using coal | Steppir up | ıg 🔶 | R&D | Impl | ementa | tion |
| Challenges common in social fundamental 2020 2030 2040 2050 2100 | | | | | | 2100 |
| Technical development of low cost and massive amount of hydrogen production, transfer and storage | R | &D | | Imple | mentati | |
| Technical development on CO2 capture and strage/usage Solving social issues (location, PA, etc.) | R | &D | | Imple | mentati | 0 |
| | A specific in iron & steel sector Raising ratio of H2-reduction in blast furnace using internal H2 (COG) Capturing CO2 from blast furnace gas for storage Further H2-reduction in blast furnace by adding H2 from outside (assuming massive carbon-free H2 supply becomes available) H2-reduction ironmaking without using coal Common in social fundamental Technical development of low cost and massive amount of hydrogen production, transfer and storage Technical development on CO2 capture and strage/usage Solving social issues (location, PA, etc.) | s specific in iron & steel sector 2020 Raising ratio of H2-reduction in blast furnace using internal H2 (COG) Capturing CO2 from blast furnace gas for storage R&D Further H2-reduction in blast furnace by adding H2 from outside (assuming massive carbon-free H2 supply becomes available) Stepping H2-reduction ironmaking without using coal Stepping Scommon in social fundamental 2020 Technical development of low cost and massive amount of hydrogen production, transfer and storage R Technical development on CO2 capture and strage/usage Solving social issues (location, PA, etc.) R | s specific in iron & steel sector 2020 2030 Raising ratio of H2-reduction in blast furnace using internal H2 (COG) Capturing CO2 from blast furnace gas for storage R&D Impl Further H2-reduction in blast furnace by adding H2 from outside (assuming massive carbon-free H2 supply becomes available) Stepping R&D H2-reduction ironmaking without using coal Stepping R&D Impl Scommon in social fundamental production, transfer and storage 2020 2030 Technical development of low cost and massive amount of hydrogen production, transfer and storage R&D Technical development on CO2 capture and strage/usage Solving social issues (location, PA, etc.) R&D | specific in iron & steel sector 2020 2030 204 Raising ratio of H2-reduction in blast furnace using internal H2 (COG) Capturing CO2 from blast furnace gas for storage R&D Implementation Further H2-reduction in blast furnace by adding H2 from outside (assuming massive carbon-free H2 supply becomes available) Stepping R&D Implementation H2-reduction ironmaking without using coal Stepping R&D R&D Implementation scommon in social fundamental production, transfer and storage 2020 2030 204 Technical development of low cost and massive amount of hydrogen production, transfer and storage R&D Implementation Technical development on CO2 capture and strage/usage Solving social issues (location, PA, etc.) R&D Implementation | a specific in iron & steel sector 2020 2030 2040 20 Raising ratio of H2-reduction in blast furnace using internal H2 (COG) Capturing CO2 from blast furnace gas for storage R&D Implementation Further H2-reduction in blast furnace by adding H2 from outside (assuming massive carbon-free H2 supply becomes available) Stepping R&D Implementation H2-reduction ironmaking without using coal Stepping R&D Implementation scommon in social fundamental production, transfer and storage 2020 2030 2040 20 Technical development of low cost and massive amount of hydrogen production, transfer and storage R&D Implementation Technical development on CO2 capture and strage/usage Solving social issues (location, PA, etc.) R&D Implementation | Specific in iron & steel sector 2020 2030 2040 2050 Raising ratio of H2-reduction in blast furnace using internal H2 (COG) Capturing CO2 from blast furnace gas for storage R&D Implementation Further H2-reduction in blast furnace by adding H2 from outside (assuming massive carbon-free H2 supply becomes available) Steppine, R&D Implementation H2-reduction ironmaking without using coal Steppine, R&D Implementation Scommon in social fundamental production, transfer and storage 2020 2030 2040 2050 Technical development of low cost and massive amount of hydrogen production, transfer and storage R&D Implementation Technical development on CO2 capture and strage/usage Solving social issues (location, PA, etc.) R&D Implementation |



COURSE50: The First Step to the Future

CO2 Ultimate Reduction in Steelmaking process by innovative technology for cool Earth 50

Ratio of reducing reaction in the experimental blast furnace



In the experimental blast furnace, 10% reduction in carbon consumption has been achieved by hydrogen-rich operation.

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Requirements for Hydrogen Supply

<u>Volume</u> for 1/2Fe₂O₃ + 3/2H₂ + 48kJ \rightarrow Fe + 3/2H₂O

reduction + compensation of endothermic reaction... 1000

Nm³-H₂/t-hot metal = 1.3 trillion Nm³-H₂/year

for worldwide iron production

<u>Cost</u> equivalent for carbon reduction ironmaking:



A trial calculation : Assuming **\$200/t-coal** and **700kg-coal/t**-hot metal, coal cost is **140\$/t**-hot metal.

55% of thermic value of coal is consumed for reduction (another 45% changes to byproduct gases), and then the cost of reducing agent is **\$77/t**-hot metal.

The equivalent cost of hydrogen (\$77/t-hot metal / 1000Nm³-H₂/t-hot metal) becomes ¢7.7/Nm³-H₂



Conclusions

✓ "A challenge towards Zero-carbon STEEL"

Direction towards achieving the long-term goal of the Paris Agreement

- Clear but very tough technical challenges
 Technical issues to overcome in hydrogen-reduction ironmaking
 Huge and stable supply of carbon-free hydrogen with rational cost
- ✓ COURSE50 : the first step to realize Zero-carbon STEEL
 - Challenge super innovative technologies for realizing Zero-carbon STEEL using the technologies gained from COURSE50



Conclusions

Carbon Recycling technology, recognizing carbon dioxide as a source of carbon, capturing and recycling it as raw materials and fuels by mineralization, artificial photosynthetic or Methanation as well as controlling the CO2 emissions to the air.
Carbon Recycling technology focuses upon the research and development of CO2 Utilization in collaboration among industries, academia and governments around the world and promotes disruptive innovation.

•Carbon Recycling is one of key technology for the world together with energy saving, renewable energy and CCS.

• Nippon Steel Corporation have several trails about CCU, for example, direct synthesis of Carbonate ester from CO2, thermal conversion to CO from CO2 for iron ore reduction, hydrogen manufacture using photosynthesis etc.

 Big challenge theme is establishing of CO2 reduction target using natural ecosystem which means creating a blue carbon ecosystem using steelmaking slag.

•We will tackle various problems surrounding ironmaking through the maximum use of the most advanced technologies and will increase Japan's world-leading energy efficiency.



Thank you very much for your kind attention

